

# Mixed iron–rhodium carbidocarbonyl clusters on oxide supports: chemistry and catalysis of syn-gas reactions

V.I. Kovalchuk\*, N.M. Mikova, N.V. Chesnokov, L.V. Naimushina, B.N. Kuznetsov

*Institute of Chemistry of Natural Organic Materials, Akademgorodok, Krasnoyarsk 660036, Russia*

## Abstract

Genesis of silica-supported  $[\text{Fe}_3\text{RhC}(\text{CO})_{16}]^-$  and  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}]^-$  clusters with interstitial carbon atoms have been investigated in CO, syn-gas and Ar media. Complete conversion of the former cluster to the latter was obtained at 50°C in any medium, with  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}]^-$  cluster yielding  $\text{Fe}_4\text{Rh}_2\text{C}(\text{CO})_{16}$  and  $[\text{Fe}_3\text{Rh}_3\text{C}(\text{CO})_{15}]^-$  mixtures at 100–150°C. Simultaneously,  $\text{Fe}^{2+}$  ions emerged on the  $\text{SiO}_2$  surface. Mössbauer and electron microscopic studies on the silica-deposited clusters showed that at treatment in any medium in the range of 250–350°C highly dispersed FeRh particles are located on the silica surface, where Fe atoms exist mainly in the oxidized state even after  $\text{H}_2$  reduction. Silica-supported catalysts derived from a family of FeRh carbidocarbonyl clusters were found to exhibit increased activity and selectivity toward oxygenates in CO hydrogenation and  $\text{C}_3\text{H}_6$  hydroformylation compared to those of monometallic cluster-derived catalysts. Possible explanations are discussed.

*Keywords:* Carbonyl clusters; Surface chemistry; Organometallic chemistry; Carbon monoxide; Hydrogenation; Hydroformylation; Supported clusters; Propylene

## 1. Introduction

Considerable advances in the synthesis of carbonyl clusters, including the heteropolynuclear ones [1] made a wide use for preparation of supported catalysts possible. Profound interest of researchers to study the catalytic behaviour of carbonyl clusters is due to their close structural [2] and chemical [3] relationship with metal surfaces covered by adsorbed CO. Hence, metal carbonyl clusters or their close precursors could be considered as active sites for the reactions of syn-gas conversion. It is known [4,5], that solid supports can stabilize some metal carbonyl clusters, espe-

cially under CO or syn-gas. These materials show catalytic activity in CO hydrogenation giving non-Schulz–Flory distribution of hydrocarbon products [5]. Some of those catalyze gas-phase olefin hydroformylation [6].

In the present paper we report the transformation of a family of silica-supported FeRh carbidocarbonyl clusters in the conditions of supported catalysts activation and their catalytic performance in CO hydrogenation and  $\text{C}_3\text{H}_6$  hydroformylation. These clusters were chosen as the catalyst precursors since supported carbonyl clusters with interstitial carbon atoms exhibited extreme stability in the conditions of CO hydrogenation and unique catalytic properties for oxygenate formation [7]. Furthermore, silica-supported catalysts derived from RhFe car-

\* Corresponding author. Tel.: (+7-391)2495387; fax: (+7-391)2439342; e-mail: kov@nchem.krasnoyarsk.su

bonyl clusters with Rh atoms dominated in a cluster framework and free from interstitial carbon atoms showed high activity and selectivity for formation of ethanol and methanol in CO hydrogenation and improved activity in hydroformylation of olefins [8,9].

## 2. Experimental

Silica (surface area,  $250 \text{ m}^2 \text{ g}^{-1}$ ) dehydrated in vacuo at  $500^\circ\text{C}$  was used as support. [TEA][ $\text{Fe}_5\text{RhC}(\text{CO})_{16}$ ] ([TEA][1]) [10], [TEA][ $\text{Fe}_4\text{RhC}(\text{CO})_{14}$ ] ([TEA][2]) [10],  $\text{Fe}_4\text{Rh}_2\text{C}(\text{CO})_{16}$  [11], [TEA][ $\text{Fe}_3\text{Rh}_3\text{C}(\text{CO})_{15}$ ] [11], [TEA] $_2$ [ $\text{Fe}_6\text{C}(\text{CO})_{16}$ ] [12] (TEA =  $\text{N}(\text{C}_2\text{H}_5)_4$ ) and  $\text{Rh}_4(\text{CO})_{12}$  [13] prepared by procedures described in the literature were used as starting materials. The deposition of cluster compounds onto  $\text{SiO}_2$  was performed under purified Ar as described previously [14]. The total metal loading for all catalysts was 2 wt.%.

The study of transformation of carbonyl clusters on the silica surface was carried out as follows. About 0.5 g of  $\text{SiO}_2$ , on which a Fe–Rh carbonyl cluster ( $\sim 50 \mu\text{mol}$  per 1 g of support) had been deposited, was heated under CO, Ar or syn-gas ( $\text{CO}:\text{H}_2 = 1:1$ ) for 2–10 h, followed by cooling to the room temperature in the medium in which the sample was treated. Then the solid was treated consecutively under Ar with 2.5 ml of dry hexane and  $\text{CH}_3\text{CN}$  or  $\text{CH}_2\text{Cl}_2$  to extract carbonyl compounds. The solid was recovered by filtration and the supernatant solution examined by infrared spectroscopy. In any case the solution was evaporated to dryness under Ar and the IR spectrum of the residue was obtained on a KBr pellet. The Rh content in the silica after extraction of carbonyl compounds was examined by X-ray fluorescence spectroscopy.

Mössbauer spectra were obtained from the solids replaced without contact with air to a cell with beryllium or magnesium windows, as described

previously [14]. Isomer shifts are given relative to sodium nitroprusside.

An electron microscopic study (TEM) was done on a JEM-100 CX instrument with 4 Å resolution as described elsewhere [15]. The size of the particles averaged for the area ( $d_s$ ) was calculated from the curves of particle size distribution obtained by statistical treatment of the micrographs.

IR spectra of solids were recorded on a Bruker IFS-113 V Fourier spectrometer within  $1300\text{--}4000 \text{ cm}^{-1}$  with a resolution of  $4 \text{ cm}^{-1}$  as described elsewhere [16]. Powdered  $\text{SiO}_2$  was pressed, forming self-supporting discs which were placed in a quartz IR cell with NaCl windows to enable an in situ deposition of FeRh clusters; the samples were treated in the cell under various gas media followed by extraction.

The CO hydrogenation reaction was performed at  $300^\circ\text{C}$  with a continuous flow copper reactor at  $300^\circ\text{C}$ , 5.0 MPa,  $\text{CO}:\text{H}_2 = 1:1$ . The space velocity was adjusted to maintain the CO conversion below 0.1%. Products were analyzed by gas chromatography.

$\text{C}_3\text{H}_6$  hydroformylation was conducted with a flow stainless steel reactor at  $200^\circ\text{C}$ , 1 atm,  $\text{CO}:\text{H}_2:\text{C}_3\text{H}_6:\text{Ar} = 1:1:1:7$  with 5% propylene conversion, as described elsewhere [17]. Steady state activity and selectivity were determined. The reaction products were analyzed by means of gas chromatography.

## 3. Results and discussion

### 3.1. The study of the transformation of $[\text{Fe}_5\text{RhC}(\text{CO})_{16}]^-$ and $[\text{Fe}_4\text{RhC}(\text{CO})_{14}]^-$ on $\text{SiO}_2$ surface by IR spectroscopic measurements

On impregnation of FeRh carbidocarbonyl cluster from acetone solution onto the degassed pellet of silica, the resulting samples gave carbonyl bands at  $2000(\text{s,br})$  and  $1850(\text{w,br})$  which resemble those of an original cluster but were broader and ill-resolved. These bands were assigned to the CO terminally and bridging-

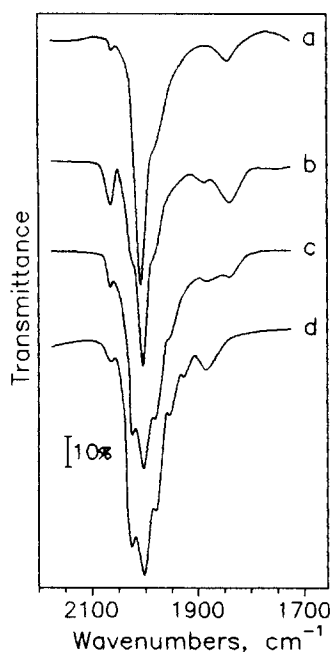


Fig. 1. Infrared spectra of (a)  $[\text{Fe}_5\text{RhC}(\text{CO})_{16}][\text{TEA}]$  in  $\text{CH}_2\text{Cl}_2$ , (b) compounds extracted with  $\text{CH}_2\text{Cl}_2$  from  $[\text{Fe}_5\text{RhC}(\text{CO})_{16}][\text{TEA}]/\text{SiO}_2$  following 2 weeks exposure under Ar at room temperature and (c) compounds extracted with  $\text{CH}_2\text{Cl}_2$  from  $[\text{Fe}_5\text{RhC}(\text{CO})_{16}][\text{TEA}]/\text{SiO}_2$  following its treatment by  $\text{CO} + \text{H}_2$  flow for 1 h at  $50^\circ\text{C}$ , (d)  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}][\text{TEA}]$  in  $\text{CH}_3\text{CN}$ .

bonded with cluster framework. The treatment of supported clusters at  $50\text{--}150^\circ\text{C}$  under  $\text{CO} + \text{H}_2$  or

$\text{CO}$  did not result in significant changes in the IR spectrum of the pellet. An extraction of sample with acetone led to complete disappearance of absorption bands in the  $\text{CO}$  stretching region. It indicates the chemical frugidity of silica surface with respect to  $\text{FeRh}$  carbonyl clusters deposited thereon.

IR spectra of individual  $[\text{TEA}][\mathbf{1}]$ ,  $[\text{TEA}][\mathbf{2}]$  and compounds extracted from  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  after treatment in Ar medium at  $20^\circ\text{C}$  and in  $\text{CO} + \text{H}_2$  flow at  $50^\circ\text{C}$  are shown in Fig. 1. Band wave numbers are listed in Table 1. The spectrum of carbonyl compounds extracted from  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  following 2 weeks exposure under Ar at  $20^\circ\text{C}$  consists of absorption bands at  $2064(\text{w})$ ,  $2024(\text{m sh})$ ,  $2004(\text{s})$ ,  $1982(\text{m sh})$ ,  $1886(\text{vw})$  and  $1841(\text{w}) \text{ cm}^{-1}$ . The bands at  $2024$  and  $1886 \text{ cm}^{-1}$  are unambiguously assigned to  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}]^- (\mathbf{2})$  [11] and those at  $2064$ ,  $2004$ ,  $1982$  and  $1841 \text{ cm}^{-1}$  to  $[\text{Fe}_5\text{RhC}(\text{CO})_{16}]^- (\mathbf{1})$ . It is worth noting that the bands at  $2062$ ,  $2002$  and  $1982 \text{ cm}^{-1}$  are also available in the IR spectrum of the former cluster. Thus, the partial conversion of  $\mathbf{1}$  into  $\mathbf{2}$  occurs under Ar at ambient temperature. Complete conversion of the former cluster to latter was obtained following treatment

Table 1

The  $\nu(\text{CO})$  vibrations of the carbonyl compounds extracted from  $\text{SiO}_2$  after treatment of deposited  $\text{FeRh}$  carbonyl clusters with syn-gas (1:1) and individual clusters in solution

Solid	Treatment	$\nu(\text{CO})$ vibrations <sup>b</sup> , $\text{cm}^{-1}$
$[\text{Fe}_5\text{RhC}(\text{CO})_{16}][\text{TEA}]^a/\text{SiO}_2$	Ar, $20^\circ\text{C}$ , 2 weeks	$2064\text{w}$ , $2024\text{m}(\text{sh})$ , $2004\text{s}$ , $1982\text{m}(\text{sh})$ , $1886\text{vw}$ , $1841\text{w}$ (methylene chloride)
	$\text{CO} + \text{H}_2$ flow, $50^\circ\text{C}$ , 1 h	$2064\text{vw}$ , $2024\text{s}$ , $2003\text{vs}$ , $1984\text{m}$ , $1956\text{w}$ , $1886\text{vw}$ , $1841\text{vw}$ (methylene chloride)
	$\text{CO} + \text{H}_2$ flow, $150^\circ\text{C}$ , 2 h	$2072\text{vw}$ , $2055\text{m}$ , $2045\text{m}$ , $2026\text{s}$ , $2000\text{vs}$ , $1982\text{m}(\text{sh})$ , $1956\text{w}$ , $1880\text{w}$ (methylene chloride)
$[\text{Fe}_5\text{RhC}(\text{CO})_{16}][\text{TEA}]/\text{SiO}_2$	$\text{CO} + \text{H}_2$ flow, $150^\circ\text{C}$ , 10 h	$2062\text{vw}$ , $2016\text{s}$ , $2002\text{sh}$ , $1980\text{m}$ , $1956\text{w}$ , $1877\text{w}$ , $1852\text{vw}$ (methylene chloride)
$[\text{Fe}_5\text{RhC}(\text{CO})_{16}][\text{TEA}]$	–	$2062\text{vw}$ , $2003\text{vs}$ , $1983\text{m}$ , $1843\text{w}$ (methylene chloride)
$[\text{Fe}_4\text{RhC}(\text{CO})_{14}][\text{TEA}]$	–	$2062\text{vw}$ , $2025\text{s}$ , $2002\text{vs}$ , $1982\text{m}$ , $1956\text{w}$ , $1930\text{vw}$ , $1880\text{w}$ (methyl cyanide)
$\text{Fe}_4\text{Rh}_2\text{C}(\text{CO})_{16}$	–	$2074\text{vw}$ , $2055\text{s}(\text{sh})$ , $2042\text{vs}$ , $2028\text{m}$ , $2018\text{m}$ , $1998\text{w}$ , $1982\text{w}$ , $1965\text{vw}$ (hexane)
$[\text{Fe}_3\text{Rh}_3\text{C}(\text{CO})_{15}][\text{TEA}]$	–	$2042\text{vw}$ , $2016\text{vs}$ , $1978\text{s}$ , $1934\text{w,br}$ , $1878\text{w}$ , $1852\text{vw}$ (methylene chloride)

<sup>a</sup>  $\text{TEA} = \text{N}(\text{C}_2\text{H}_5)_4$ .

<sup>b</sup> br = broad peak, s = strong intensity, vs = very strong, m = medium, w = weak, vw = very weak, sh = shoulder.

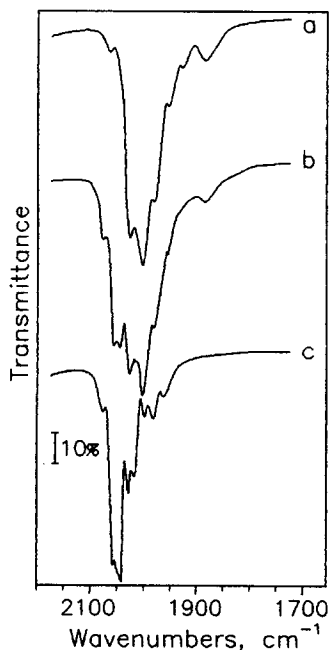


Fig. 2. Infrared spectra of (a)  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}][\text{TEA}]$  in  $\text{CH}_3\text{CN}$ , (b) compounds extracted with  $\text{CH}_2\text{Cl}_2$  from  $[\text{Fe}_3\text{RhC}(\text{CO})_{16}][\text{TEA}]/\text{SiO}_2$  following its treatment by  $\text{CO} + \text{H}_2$  flow for 2 h at  $150^\circ\text{C}$ , (c)  $\text{Fe}_4\text{Rh}_2\text{C}(\text{CO})_{16}$  in  $\text{CH}_2\text{Cl}_2$ .

of the  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  sample by syn-gas for 1 h at  $50^\circ\text{C}$ . In this case infrared bands of carbonyl compounds extracted from the solid coincide in fact with those of individual **2** (Table 1). Only a band at  $1841\text{ cm}^{-1}$  indicates that small amounts of **1** are still present in the solution.

Rhodium was not detected by X-ray fluorescence analysis of the  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  sample after its thermolysis both in syn-gas and Ar medium followed by extraction of carbonyl compounds. This shows that transformation of **1** to **2** occurs with very high selectivity. It is worth noting that conversion of **1** to **2** in solution is well known [11,18]. However, the selectivity of the process in these cases was equal to 70% when the reaction was carried out in diglyme media [11] and 92% towards the mixture of **2** and  $\text{Fe}_4\text{Rh}_2\text{C}(\text{CO})_{16}$  which was derived from **1** in the conditions of liquid-phase hydroformylation of pentene-1 ( $100^\circ\text{C}$ , 60 atm,  $1\text{CO} + 1\text{H}_2$ ) [18].

Infrared bands at  $2072(\text{vw})$ ,  $2055(\text{m})$ ,  $2045(\text{m})$ ,  $2026(\text{s})$ ,  $2017(\text{sh})$ ,  $2000(\text{vs})$ ,  $1982(\text{m sh})$ ,  $1956(\text{w})$  and  $1880(\text{w})\text{ cm}^{-1}$  (Fig. 2, Table 1) were observed in IR spectra of

carbonyl compounds extracted from  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  following treatment in  $\text{CO} + \text{H}_2$  flow at  $150^\circ\text{C}$  for 2 h. The bands at  $2026$ ,  $2000$ ,  $1982$ ,  $1956$  and  $1880\text{ cm}^{-1}$  are assigned to **2** [11] and those at  $2072$ ,  $2055$ ,  $2045$ ,  $2026$  and  $1982\text{ cm}^{-1}$  to  $\text{Fe}_4\text{Rh}_2\text{C}(\text{CO})_{16}$ . These measurements show the absence of initial cluster in the extract. Only trace amounts of rhodium on silica following extraction were found by means of X-ray fluorescence spectroscopy. Increasing the exposure of  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  in syn-gas flow at  $150^\circ\text{C}$  up to 5 h resulted in the appearance in the extract of  $[\text{Fe}_3\text{Rh}_3\text{C}(\text{CO})_{15}]^-$ . This cluster was identified by infrared spectroscopy of KBr pellets of the residue obtained by evaporation of the extract to dryness. The thermolysis of  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  under Ar at  $150^\circ\text{C}$  led to similar changes as under syn-gas. However, in this case negligible amounts of Rh were detected on silica surface following extraction with  $\text{CH}_2\text{Cl}_2$ .

The treatment of  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  sample at  $250^\circ\text{C}$  for 2 h resulted in complete decarbonylation of supported cluster under any gas medium.

Silica supported **2** was not markedly transformed in flowing  $\text{CO} + \text{H}_2$  at temperatures below  $150^\circ\text{C}$ . The bands which do not relate to **2** were revealed by infrared spectroscopy of the solution obtained by extraction with  $\text{CH}_2\text{Cl}_2$  from  $[\text{TEA}][\mathbf{2}]/\text{SiO}_2$  only following treatment in flowing syn-gas at  $150^\circ\text{C}$  for 3 h. At 10 h exposure of supported cluster infrared bands of the solution were observed at  $2062(\text{vw})$ ,  $2016(\text{s})$ ,  $2002(\text{sh})$ ,  $1980(\text{m})$ ,  $1956(\text{w})$ ,  $1877(\text{w})$  and  $1852(\text{vw})\text{ cm}^{-1}$  (Fig. 3, Table 1). The band at  $2016$  and two bands at  $1878$  and  $1850$  assigned to bridging-bonded CO [11] indicate unambiguously that transformation of **2** into  $[\text{Fe}_3\text{Rh}_3\text{C}(\text{CO})_{15}]^-$  hexanuclear cluster occurs on the silica surface.

It is worth noting that none of the IR spectra of carbonyl compounds extracted had absorption bands which could be assigned to homonuclear clusters of Fe or Rh.

### 3.2. $^{57}\text{Fe}$ Mössbauer spectroscopy data

The valence state of Fe in individual **1** and in **1** deposited on silica followed by exposure in

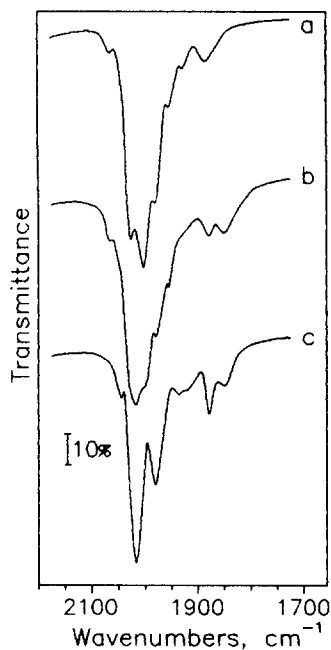


Fig. 3. Infrared spectra of (a)  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}][\text{TEA}]$  in  $\text{CH}_3\text{CN}$ , (b) compounds extracted with  $\text{CH}_2\text{Cl}_2$  from  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}][\text{TEA}]/\text{SiO}_2$  following its treatment by  $\text{CO} + \text{H}_2$  flow for 10 h at  $150^\circ\text{C}$ , (c)  $[\text{Fe}_3\text{Rh}_3\text{C}(\text{CO})_{15}][\text{TEA}]$  in  $\text{CH}_2\text{Cl}_2$ .

$\text{CO} + \text{H}_2$  flow at different temperatures was studied by Mössbauer spectroscopy. The Mössbauer spectrum of individual **1** was resolved into two pairs of quadrupole doublets (I.S., Q.S. = 0.33, 0.57 and 0.50, 0.94 mm/s, respectively) by computer fitting. It suggests that iron atoms occupy chemically unequivalent positions in the cluster framework. Most likely these are the *cis*- and *trans*-positions relative to rhodium atoms in octahedral **1**, taking into account that the ratio of the peak areas of  $\text{Fe}^0/\text{Fe}^0$  was 4.

Depositing  $[\text{TEA}][\mathbf{1}]$  on silica surface led to the additional pair of quadrupole doublets assigned to  $\text{Fe}^{2+}$  (I.S. = 1.26, Q.S. = 2.28 mm/s). The relative contribution of this iron state into the integral spectrum increased following treatment of  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  sample by flowing syn-gas at  $50^\circ\text{C}$ . At moderate temperature and in the absence of oxygen the appearance of  $\text{Fe}^{2+}$  ions on silica surface could be due to the oxidation of Fe atoms eliminated from **1** by surface OH-groups [19–21]. When the temperature of the treatment of  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  sample by syn-gas increases from  $50^\circ\text{C}$  to  $150^\circ\text{C}$ , the  $\text{Fe}^{2+}$  peak area increases

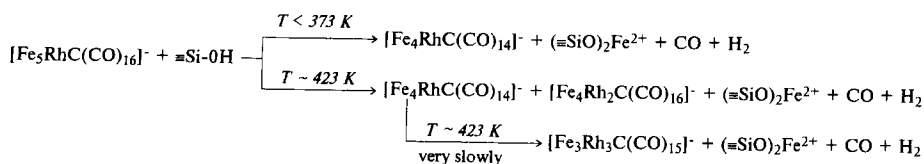
too. As evidenced by IR spectroscopy data, supported **1** transforms into mixtures of **2** and  $\text{Fe}_4\text{Rh}_2\text{C}(\text{CO})_{16}$  at  $150^\circ\text{C}$ . Formation of the last cluster could result in additional releases of Fe which could be oxidized by silica surface.

The treatment of silica supported **1** by syn-gas at  $250^\circ\text{C}$  resulted in complete decomposition of carbonyl compounds and hydrocarbon formation was observed at these conditions. Simultaneously  $\text{Fe}^{3+}$  (I.S. = 0.65, Q.S. = 0.90 mm/s) emerged on the support. Reduction of  $[\text{TEA}][\mathbf{1}]/\text{SiO}_2$  sample by  $\text{H}_2$  led to an increase of the  $\text{Fe}^0$  surface area in Mössbauer spectra and corresponding decrease in  $\text{Fe}^{2+}$  surface area. The  $\text{Fe}^{3+}$  fraction in this case remained almost the same compared to that for sample treated by syn-gas at  $250^\circ\text{C}$ .

From the preceding transformation of silica supported **1** at the temperature  $\leq 150^\circ\text{C}$  can schematically be described in Scheme 1. Although in the present research there was no attempt to detect gaseous products during supported clusters transformation, they should be formed for mass balance and they were found in [19–21] where related transformations were studied. Since no homonuclear carbidocarbonyl iron clusters were revealed in the process of thermolysis of supported FeRh clusters, the fate of interstitial carbon atom remains unclear and needs further investigation. These atoms may form iron carbides in an inert atmosphere or hydrocarbons in the presence of hydrogen.

### 3.3. Electron microscopy study

The study of reduced at  $350^\circ\text{C}$  catalysts derived from FeRh carbonyl clusters with electron microscopy showed that all samples contained homogeneous metal particles with the size of ca. 0.5 nm. This value is close to the size of hexanuclear cluster framework [11]. Reduced at  $350^\circ\text{C}$   $\text{Rh}_4/\text{SiO}_2$  derived from  $\text{Rh}_4(\text{CO})_{12}$  contained Rh particles with a mean size of ca. 2.5 nm. Thus, small sizes and homogeneity of bimetallic particles in reduced catalysts along with the possibility of stabilization of small metal clusters on anchored ions, as reported elsewhere [22], suggests that reduced



Scheme 1.

catalysts involve dispersed FeRh particles which interact with  $\text{Fe}^{n+}$  ions bound chemically with the surface of silica.

### 3.4. CO hydrogenation on FeRh carbonyl cluster derived catalysts

The results of CO hydrogenation at 5.0 MPa are summarized in Table 2. All the catalysts had initially higher rates for hydrocarbons and lower rates for oxygenates, but changed gradually to oxygenate-producing catalysts. In each case, the catalytic activity slightly increased for the first 2–5 h on stream, then reached a steady state and remained constant for many subsequent hours.

$\text{Rh}_4/\text{SiO}_2$  catalysts prepared from  $\text{Rh}_4(\text{CO})_{12}$  produced hydrocarbons  $\text{C}_1$ – $\text{C}_5$  with 87% selectivity. The selectivity toward oxygenates in products was 13%; mainly methanol was obtained and some amounts of ethanol and propanol were produced.  $\text{Fe}_6\text{C}/\text{SiO}_2$  prepared from an anion cluster

$[\text{Fe}_6\text{C}(\text{CO})_{16}][\text{TEA}]_2$  demonstrated surprisingly high selectivity toward ethanol which reached 13% with 20% toward oxygenates in general. Among hydrocarbon products  $\text{C}_3$ – $\text{C}_4$  olefins prevailed. On all FeRh bimetallic catalysts with the exception of  $\text{Fe}_5\text{RhC}/\text{SiO}_2$  prepared from  $[\text{Fe}_5\text{RhC}(\text{CO})_{16}][\text{TEA}]$  selectivities for oxygenates were substantially increased. Notably, the selectivity toward ethanol was strikingly increased on  $\text{Fe}_4\text{RhC}/\text{SiO}_2$  and reached to 38%. Overall selectivity toward oxygenates on this catalyst was more than 70%. Increased selectivity toward methanol was observed for  $\text{Fe}_3\text{Rh}_3\text{C}/\text{SiO}_2$  and  $\text{Fe}_4\text{Rh}_2\text{C}/\text{SiO}_2$  catalysts. The feature of the latter catalyst is the marked formation of propanol. The FeRh catalysts promote methane formation as well, but relative enhancement of rates for oxygenates was much higher than for methane. Accordingly, the selectivities toward hydrocarbons  $\text{C}_{2+}$  were decreased from 66% for  $\text{Rh}_4/\text{SiO}_2$  and 59% for  $\text{Fe}_6\text{C}/\text{SiO}_2$  to less than 3% for

Table 2

CO Hydrogenation on  $\text{SiO}_2$ -supported Rh, RhFe and Fe carbonyl cluster-derived catalysts<sup>a</sup>

Precursor/ $\text{SiO}_2$	At. ratio Fe/Rh	Total specific activity <sup>b</sup>	Selectivity (wt.%) <sup>c,d</sup>					
			$\text{CH}_4$	$\text{C}_2$ – $\text{C}_3$	$\text{C}_{3+}$	$\text{CH}_3\text{OH}$	$\text{C}_2\text{H}_5\text{OH}$	$\text{C}_{3+}\text{OH}$
$\text{RhCl}_3 \cdot 3\text{H}_2\text{O}$	0	68	29	55	16	0	0	0
$\text{FeCl}_3$	$\infty$	27	28	45	27	0	0	0
$\text{RhCl}_3 \cdot 3\text{H}_2\text{O} + \text{FeCl}_3$	4	22	87	9	4	0	0	0
$\text{Rh}_4(\text{CO})_{12}$	0	235	21	22	44	8	2	3
$[\text{Rh}_3\text{Fe}_3\text{C}(\text{CO})_{15}][\text{TEA}]$	1	8 <sup>e</sup>	40	8	1	28	16	6
$\text{Rh}_2\text{Fe}_4\text{C}(\text{CO})_{16}$	2	11 <sup>e</sup>	55	7	1	15	5	17
$[\text{RhFe}_4\text{C}(\text{CO})_{14}][\text{TEA}]$	4	267 <sup>e</sup>	24	2	<1	33	38	2
$[\text{RhFe}_5\text{C}(\text{CO})_{16}][\text{TEA}]$	5	37	76	7	3	12	1	<1
$[\text{Fe}_6\text{C}(\text{CO})_{16}][\text{TEA}]_2$	$\infty$	17	21	33	26	5	13	2

<sup>a</sup> Reaction conditions: catalyst 0.3 g, total metal loading 2 wt.%, reaction temperature  $300^\circ\text{C} \pm 2^\circ\text{C}$ ,  $\text{CO}/\text{H}_2 = 1$ , total pressure  $5.0 \times 10^6$  Pa, space velocity  $1000 \text{ h}^{-1}$ , prior to catalytic run all the catalysts were reduced by  $\text{H}_2$  at  $325^\circ\text{C}$  for 1 h.

<sup>b</sup>  $\text{mmol}_{\text{CO}} \cdot (\text{mol}_{\text{Rh}+\text{Fe}})^{-1} \text{ h}^{-1}$  in 2 h on stream.

<sup>c</sup> Selectivities were calculated in 2 h on stream as follows:  $100 \times C_i / \sum C_i$ ,  $i$  = carbon number of the product molecule,  $C_i$  = weight concentration of the product molecule.

<sup>d</sup>  $\text{C}_{3+}$ , hydrocarbons with more than 3 carbon atoms in a molecule,  $\text{C}_{3+}\text{OH}$ , oxygenates with more than 3 carbon atoms in a molecule.

<sup>e</sup> In 5 h on stream.

$\text{Fe}_4\text{RhC}/\text{SiO}_2$ . The latter catalyst had the highest catalytic activity, which exceeded that of  $\text{Rh}_4/\text{SiO}_2$ . The activities of other FeRh catalysts were similar to or even less than that of the  $\text{Fe}_6\text{C}/\text{SiO}_2$  sample. The reason for this is unclear and needs further investigation. The salt-derived (Fe–Rh)/ $\text{SiO}_2$  catalyst showed decreased activity and selectivity to oxygenates compared to that on  $\text{Fe}_4\text{RhC}/\text{SiO}_2$  at the same Fe/Rh ratio of 4.0.

### 3.5. Hydroformylation of propylene on FeRh cluster-derived catalysts

There is some analogy between olefin hydroformylation and  $\text{C}_{2+}$ -oxygenate synthesis from  $\text{CO} + \text{H}_2$  mixture. Oxygenates in the latter reaction appear to result from migratory insertion of CO adsorbed into the bond between surface metal atom and surface alkyl formed in turn from adsorbed CO and  $\text{H}_2$  by the consequence of elementary steps [23–26]. The key step of olefin hydroformylation is also migratory CO insertion [27]. Hence, this reaction can be chosen to evaluate the ability of active sites for CO insertion.

The results of propylene hydroformylation on silica-supported FeRh cluster-derived catalysts are provided by Table 3. In all runs, the activity reached the steady state after 4–6 h on stream and remained constant for many subsequent hours.

Under the reaction conditions of 200°C and 0.1 MPa hydrogenation of propylene to propane dominates over hydroformylation on  $\text{Rh}_4/\text{SiO}_2$ . The selectivity toward oxygenates is only 17%. On  $\text{Fe}_6\text{C}/\text{SiO}_2$  derived from  $[\text{Fe}_6\text{C}(\text{CO})_{16}][\text{TEA}]_2$ , neither hydroformylation nor hydrogenation were observed under the reaction parameters used.

The activity for hydroformylation on the catalysts derived from FeRh carbidocarbonyl clusters was increased. For example, the rate for oxygenates for  $\text{Fe}_4\text{RhC}/\text{SiO}_2$  was improved by factor 6 compared with  $\text{Rh}_4/\text{SiO}_2$  sample. All the FeRh catalysts with the exception of  $\text{Fe}_4\text{RhC}/\text{SiO}_2$  showed suppressed rates for hydrogenation of propylene. Thus, the selectivity toward oxygenates was substantially increased on the FeRh catalysts: 17% on the  $\text{Rh}_4/\text{SiO}_2$ , 40–47% on the FeRh/ $\text{SiO}_2$ . Mainly propanol-1 was obtained on the FeRh catalysts, although  $\text{Rh}_4/\text{SiO}_2$  gave only aldehydes as oxygenates. The selectivity toward normal isomer of oxygenates was slightly affected by the Fe/Rh ratio in initial clusters: it was 77% on  $\text{Rh}_4/\text{SiO}_2$  and 65–75% on FeRh cluster-derived catalysts. This implies that Fe does not produce steric hindrance around Rh to insert CO into metal–alkyl bond on the surface of a catalyst.

Thus, the propylene hydroformylation study suggests that supported FeRh carbidocarbonyl clusters could provide mixed FeRh sites which

Table 3  
Hydroformylation of propylene on  $\text{SiO}_2$ -supported Rh, RhFe and Fe carbonyl cluster-derived catalysts<sup>a</sup>

Precursor/ $\text{SiO}_2$	At. ratio Fe/Rh	Specific rate of formation <sup>b</sup> , $\text{h}^{-1}$		Selectivity, mol%		
		$\text{C}_3\text{H}_8$	PrCHO + BuOH <sup>c</sup>	Oxygenates <sup>d</sup>	Alcohol <sup>e</sup>	<i>n</i> -Isomer <sup>f</sup>
$\text{Rh}_4(\text{CO})_{12}$	0	3.27	0.66	17	0	77
$[\text{Rh}_3\text{Fe}_3\text{C}(\text{CO})_{15}][\text{TEA}]$	1	1.26	0.84	40	74	75
$\text{Rh}_2\text{Fe}_4\text{C}(\text{CO})_{16}$	2	2.99	2.72	47	66	72
$[\text{RhFe}_4\text{C}(\text{CO})_{14}][\text{TEA}]$	4	4.47	3.82	46	78	68
$[\text{RhFe}_5\text{C}(\text{CO})_{16}][\text{TEA}]$	5	1.43	0.96	40	70	65
$[\text{Fe}_6\text{C}(\text{CO})_{16}][\text{TEA}]_2$	$\infty$	0	0			

<sup>a</sup> Reaction conditions: catalyst 0.3 g, total metal loading 2 wt.%, reaction temperature 200°C  $\pm$  2°C,  $\text{C}_3\text{H}_6/\text{CO}/\text{H}_2/\text{Ar} = 1/1/1/7$ , total pressure  $1 \times 10^5$  Pa, prior to catalytic run all the catalysts were reduced by  $\text{H}_2$  at 300°C for 1 h.

<sup>b</sup>  $\text{mol}_{\text{CO}} \cdot (\text{mol}_{\text{Rh} + \text{Fe}})^{-1} \text{h}^{-1}$ .

<sup>c</sup> *n*- and *i*-butanal + *n*- and *i*-butanol.

<sup>d</sup>  $(\text{PrCHO} + \text{BuOH}) / (\text{C}_3\text{H}_8 + \text{PrCHO} + \text{BuOH}) \times 100$ .

<sup>e</sup>  $\text{BuOH} / (\text{PrCHO} + \text{BuOH})$ .

<sup>f</sup>  $(\text{n-PrCHO} + \text{n-BuOH}) / (\text{PrCHO} + \text{BuOH}) \times 100$ .

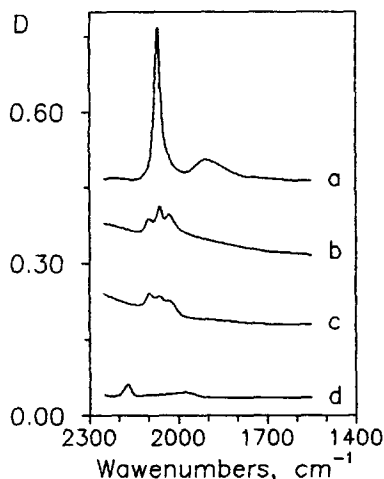


Fig. 4. FTIR spectra of CO adsorbed at 0.45 Torr pressure on (a)  $\text{Rh}_4/\text{SiO}_2$ , (b)  $\text{Fe}_4\text{RhC}/\text{SiO}_2$ , (c)  $\text{Fe}_3\text{RhC}/\text{SiO}_2$  and (d)  $\text{Fe}_6\text{C}/\text{SiO}_2$  following  $\text{H}_2$  reduction at  $350^\circ\text{C}$  for 1 h.

have increased activity for hydroformylation. It is worth noting that similar results were obtained by M. Ichikawa et al. on silica-supported RhFe catalysts derived from RhFe clusters free from interstitial carbon atoms [8,9].

### 3.6. FTIR spectroscopy of adsorbed CO

FTIR studies of adsorbed CO were carried out for  $\text{Rh}_4/\text{SiO}_2$ ,  $\text{Fe}_3\text{RhC}/\text{SiO}_2$ ,  $\text{Fe}_4\text{RhC}/\text{SiO}_2$  and  $\text{Fe}_6\text{C}/\text{SiO}_2$  following  $\text{H}_2$  reduction at  $350^\circ\text{C}$ . In the presence of CO, bands due to three CO species were observed (Fig. 4): a linear species at  $2072$  ( $\text{Rh}_4/\text{SiO}_2$ ),  $2062$  ( $\text{FeRhC}/\text{SiO}_2$ ) and  $1970$   $\text{cm}^{-1}$  ( $\text{Fe}_6\text{C}/\text{SiO}_2$ ), a bridged species at  $1920$   $\text{cm}^{-1}$  ( $\text{Rh}_4/\text{SiO}_2$ ) and a geminal dicarbonyl species with twin bands at  $2095$  and  $2035$   $\text{cm}^{-1}$  ( $\text{FeRhC}/\text{SiO}_2$ ). Besides, the relative intensities of the linear species to the geminal dicarbonyl ones in the spectrum of  $\text{Fe}_3\text{RhC}/\text{SiO}_2$  are appreciably suppressed compared to  $\text{Fe}_4\text{RhC}/\text{SiO}_2$ . In addition, a band at  $2170$   $\text{cm}^{-1}$  was observed for the  $\text{Fe}_6\text{C}/\text{SiO}_2$  catalyst. The bridging CO band in  $\text{FeRhC}/\text{SiO}_2$  catalysts was completely suppressed. It is worth noting that no low-frequency bands within  $1600$ – $1650$   $\text{cm}^{-1}$  were revealed in  $\text{FeRhC}/\text{SiO}_2$  catalysts. A low-frequency band appeared at ca.  $1630$   $\text{cm}^{-1}$  in  $\text{RhFe}/\text{SiO}_2$  catalysts derived from RhFe carbonyl clusters free of inter-

stitial carbon atoms [8,9] was attributed to C- and O-bonded CO on mixed  $\text{Rh-Fe}^{3+}$  sites. M. Ichikawa et al. [8,9] suggested that increased activity of such  $\text{RhFe}/\text{SiO}_2$  catalysts toward oxygenates is due to the two-site activation of CO with  $\text{Rh-Fe}^{3+}$  to enhance the migratory CO insertion into  $\text{Rh-H}$  and  $\text{Rh-alkyl}$  and enhance the hydrogenation of resulting formyl or acetyl complexes to methanol or ethanol. However,  $\text{Fe}_4\text{RhC}/\text{SiO}_2$  catalysts derived from carbidocarbonyl  $[\text{Fe}_4\text{RhC}(\text{CO})_{16}]^-$  cluster exceeds  $\text{Rh}_4/\text{SiO}_2$  in activity. Most of the  $\text{FeRhC}/\text{SiO}_2$  and  $\text{Fe}_6\text{C}/\text{SiO}_2$  catalysts exhibit higher selectivity toward oxygenates compared to that of  $\text{Rh}_4/\text{SiO}_2$ . This indicates that the availability of the two-site activated CO is necessary to provide enhanced activity of a supported metal catalyst. For example, terminal CO adsorbed on  $\text{Rh}^+$  was demonstrated to be highly capable in migratory insertion [28]. Perhaps, as for  $\text{FeRhC}/\text{SiO}_2$  catalysts, electron interaction between Rh, Fe and carbide C might have a dominant effect on the catalytic properties in the syn-gas reactions. The research to verify this assumption are in progress.

## 4. Conclusion

The transformation of silica-supported  $[\text{Fe}_5\text{RhC}(\text{CO})_{16}]^-$  and  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}]^-$  clusters with interstitial carbon atoms have been investigated in CO, syn-gas and Ar media. Complete conversion of the former cluster to the latter was obtained at  $50^\circ\text{C}$  in any medium, with  $[\text{Fe}_4\text{RhC}(\text{CO})_{14}]^-$  cluster yielding  $\text{Fe}_2\text{Rh}_4\text{C}(\text{CO})_{16}$  and  $[\text{Fe}_3\text{Rh}_3\text{C}(\text{CO})_{15}]^-$  mixture at  $100$ – $150^\circ\text{C}$ . Simultaneously  $\text{Fe}^{2+}$  ions emerged on the  $\text{SiO}_2$  surface. Mössbauer and electron microscopic studies on the silica-deposited clusters showed that at treatment in any medium in the range of  $250$ – $350^\circ\text{C}$  highly dispersed FeRh particles are located on the silica surface, where Fe atoms exist mainly in the oxidized state even after  $\text{H}_2$  reduction. Silica-supported catalysts derived from FeRh carbidocarbonyl clusters were found to exhibit increased activity and selectivity



toward oxygenates in CO hydrogenation and C<sub>3</sub>H<sub>6</sub> hydroformylation compared to those of mono-metallic cluster-derived catalysts. This activity and selectivity might be due to electron interaction between Rh, Fe and carbide C.

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